Application No.: Not Yet Assigned Docket No.: 12810-00085-US

## **AMENDMENTS TO THE CLAIMS**

The listing of claims will replace all prior versions, and listings, of claims in the application.

 (Currently Amended) A process for purifying crude caprolactam which has been obtained by-comprising

- 1) converting a mixture (I) comprising 6-aminocapronitrile and water to a mixture (II) comprising caprolactam, ammonia, water, high boilers and low boilers in the presence of a catalyst, then
- 2) removing ammonia from <u>the</u> mixture (II) to obtain a mixture (III) comprising caprolactam, water, high boilers and low boilers, then
- 3) completely or partly removing water from the mixture (III) to obtain crude caprolactam (IV) comprising caprolactam, high boilers and low boilers, and
- 4) which comprises distilling the crude caprolactam (IV) comprising
  - a) feeding the crude caprolactam (IV) and an inorganic acid which has a boiling point above the boiling point of caprolactam under the distillation conditions of the following steps b) to h) to a first distillation apparatus C1,
  - b) distilling the crude caprolactam <u>IV</u> and the inorganic acid in the first distillation apparatus C1, and removing a first substream in the bottom region and a second substream in the top region of the distillation apparatus C1,
  - c) feeding the second substream from step b) to a second distillation apparatus C2,
  - d) distilling the second substream from step b) in the second distillation apparatus
     C2, and removing a first substream in the bottom region and a second
     substream in the top region of the distillation apparatus C2,
  - e) feeding the first substream from step d) to a third distillation apparatus C3,

Application No.: Not Yet Assigned Docket No.: 12810-00085-US

f) distilling the first substream from d) in the third distillation apparatus C3, and removing a first substream in the bottom region and purified caprolactam in the top region of distillation apparatus C3, and

- g) feeding the first substream from step f) to the first distillation apparatus C1.
- 2. (Currently Amended) A process as claimed in claim 1, wherein mixture (I) additionally further comprises an organic liquid diluent.
- 3. (Original) A process as claimed in claim 2, wherein the liquid diluent is removed in step 3), before, during or after the removal of water from mixture (III).
- 4. (Currently Amended) A process as claimed in any of claims 1 to 3 claim 1, wherein low boilers are removed or high boilers are removed or low boilers and high boilers are removed between step 3) and step 4a).
- 5. (Original) A process as claimed in claim 4, wherein first low boilers and then high boilers are removed.
- 6. (Currently Amended) A process as claimed in claim 4 or 5, wherein 6-aminocapronitrile is removed as a low boiler.
- 7. (Currently Amended) A process as claimed in any of claims 1 to 6 claim 1, wherein the inorganic acid used is phosphoric acid.
- 8. (Currently Amended) A process as claimed in any of claims 1 to 7 claim 1, wherein the weight ratio of the substream comprising purified caprolactam removed in the top region to the substream removed in the bottom region in step f) of the distillation apparatus C3 is in the range from 0.3 to 2.0.
- 9. (Currently Amended) A process as claimed in any of claims 1 to 8 claim 1, wherein at least a portion of the first substream obtained in step b) is mixed with the crude caprolactam according to the preamble (IV).

Application No.: Not Yet Assigned Docket No.: 12810-00085-US

10. (Currently Amended) A process as claimed in claim 9, wherein the weight ratio of the <u>first</u> substream <u>obtained from the distillation apparatus C1that is mixed</u> with the crude caprolactam (IV) to crude caprolactam is in the range from 0.01 to 0.3.

- 11. (Currently Amended) A process as claimed in any of claims 1 to 10 claim 1, wherein at least a portion of the second substream obtained in step d) from the distillation apparatus
  C2 is recycled in step 3) before the low boilers are removed.
- 12. (Currently Amended) A process as claimed in any of claims 1 to 11 claim 1, wherein the bottom temperature in the distillation apparatus C1 is in the range from 120 to 200°C.
- 13. (Currently Amended) A process as claimed in any of claims 1 to 12 claim 1, wherein the pressure in one, two or three of distillation apparatus C1, C2, C3 is at least 40 bar, measured in the top region/bottom region.
- 14. (Currently Amended) A process as claimed in any of claims 1 to 13 claim 1, wherein the first substream from step f) distillation apparatus C3 is introduced at the top of the distillation apparatus C1.
- 15. (New) A process as claimed in claim 8, wherein the inorganic acid used is phosphoric acid.
- 16. (New) A process as claimed in claim 8, wherein at least a portion of the second substream obtained from the distillation apparatus C2 is recycled in step 3) before the low boilers are removed.
- 17. (New) A process as claimed in claim 10, wherein at least a portion of the second substream obtained from the distillation apparatus C2 is recycled in step 3) before the low boilers are removed.